

(1) + (2) + (3) =>

$$p_0 - p_3 = -\rho_{Hg} g h - \rho_0 g d_1 - \rho_v g d_2 \quad (4)$$

$$h = \frac{p_0 - p_3 + g(\rho_0 d_1 + \rho_v d_2)}{-\rho_{Hg} g}$$

överttrycket: $p_3 - p_0 = \frac{F}{A} \quad (5)$

(5) i (4) =>

$$h = \frac{-F/A + g(\rho_0 d_1 + \rho_v d_2)}{-\rho_{Hg} g} = \underline{\underline{0,44 \text{ m}}}$$

Trycket varierar linjärt över plattan; medeltrycket blir då lika med trycket i mitten p_3

$\rho_v = 998 \text{ kg/m}^3 \quad d_1 = 0,6 \text{ m}$
 $\rho_0 = 891 \text{ kg/m}^3 \quad d_2 = 0,65 \text{ m}$
 $\rho_{Hg} = 13550 \text{ kg/m}^3$

$$p_0 - p_1 = -\rho_{Hg} g (z_0 - z_1) \quad (1)$$

$$p_1 - p_2 = -\rho_0 g (z_1 - z_2) \quad (2)$$

$$p_2 - p_3 = -\rho_v g (z_2 - z_3) \quad (3)$$

givet: $L=5 \text{ m}, b=1 \text{ m}, h=1 \text{ cm}, F=850 \text{ N}$, oil SAE 50
 sökt: v

$$F = -\tau \cdot A = -\tau \cdot 2 \cdot L \cdot b \Rightarrow \tau = \frac{-F}{2 \cdot L \cdot b} = -85 \text{ N/m}^2 \quad (= \mu \frac{\partial v}{\partial x})$$

N.S. i y-rikt. (endast 2-dim strömning)

$$\frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} = -\frac{1}{\rho} \frac{\partial p}{\partial y} + g_y + \nu \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} + \frac{\partial^2 v}{\partial z^2} \right)$$

stationärt: $\frac{\partial v}{\partial t} = 0$; "lång kanal": $u=0, w=0, \frac{\partial v}{\partial y} = 0, \frac{\partial v}{\partial z} = 0, \frac{\partial^2 v}{\partial y^2} = 0, \frac{\partial^2 v}{\partial z^2} = 0$

Besökna trycket: $\frac{\partial p}{\partial y} = 0$
 $\Rightarrow 0 = g_y + \nu \frac{\partial^2 v}{\partial x^2} \Rightarrow \frac{\partial^2 v}{\partial x^2} = -\frac{g_y}{\nu}$

integrera:
 $\frac{\partial v}{\partial x} = -\frac{g_y}{\nu} x + C_1 \quad (1)$

integrera:
 $v = -\frac{g_y}{\nu} \frac{x^2}{2} + C_1 x + C_2 \quad (2)$

R.V. 1: $x=0 \quad \mu \frac{\partial v}{\partial x} = \tau \Rightarrow \frac{\partial v}{\partial x} = \frac{\tau}{\mu}$

(1) $\Rightarrow \frac{\tau}{\mu} = -\frac{g_y}{\nu} x + C_1 \Rightarrow C_1 = \frac{\tau}{\mu}$

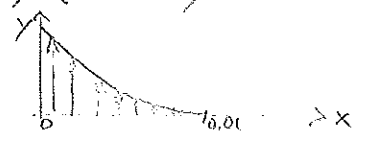
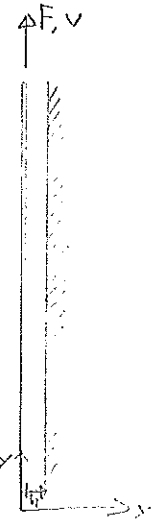
R.V. 2: $x=0,01 \text{ m} \quad v=0$

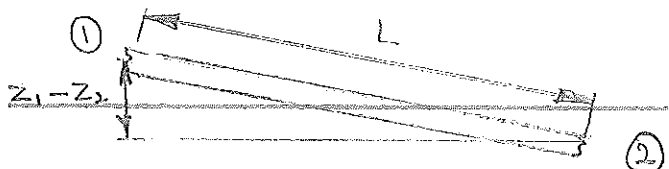
(2) $\Rightarrow 0 = -\frac{g_y}{\nu} \frac{0,01^2}{2} + \frac{\tau}{\mu} \cdot 0,01 + C_2 \Rightarrow C_2 = \frac{g_y}{\nu} \frac{0,01^2}{2} - \frac{\tau}{\mu} \cdot 0,01$

$$\Rightarrow v = -\frac{g_y}{\nu} \frac{x^2}{2} + \frac{\tau}{\mu} x + \frac{g_y}{\nu} \frac{0,01^2}{2} - \frac{\tau}{\mu} \cdot 0,01 = \frac{g_y}{\nu} (0,01^2 \cdot x^2) + \frac{\tau}{\mu} (x - 0,01)$$

$v(x=0) = 0,47 \text{ m/s}$

$\rho = 902 \text{ kg/m}^3$
 $\mu = 0,86 \text{ kg/m} \cdot \text{s}$
 $\nu = 9,534 \cdot 10^{-7} \text{ m}^2/\text{s}$





Givet: $d = 0,14 \text{ m}$ $p_1 = 150 \text{ kPa}$
 $L = 320 \text{ m}$ $p_2 = 120 \text{ kPa}$
 $z_1 - z_2 = 4,5 \text{ m}$
 $t = 10^\circ \text{C}$
 $Q_a = 1100 \text{ m}^3/\text{h} = \frac{11}{36} \text{ m}^3/\text{s}$
 $Q_b = 1,4 Q_a$

Lösning: B_s utvidgade ekv (3.68b) eller (3.78) eller (6.24)

$$p_1 + \rho \frac{v_1^2}{2} + \rho g z_1 = p_2 + \rho \frac{v_2^2}{2} + \rho g z_2 + \Delta p_f$$

$$v_1 = v_2, \quad d_1 = d_2$$

a) $\Delta p_f = p_1 - p_2 + \rho g (z_1 - z_2) = (1,5 - 1,2) \cdot 10^5 + \rho g \cdot 4,5$

Kylvatten, $t = 10^\circ \text{C} \Rightarrow \rho = 10^3 \text{ kg/m}^3$
 $\nu = 1,31 \cdot 10^{-6} \text{ m}^2/\text{s}$

$$\Delta p_f = 0,3 \cdot 10^5 + 10^3 \cdot 9,81 \cdot 4,5 = 0,74 \cdot 10^5 \text{ Pa}$$

(6.30b):

$$\Delta p_f = f \frac{L}{d} \frac{\rho V^2}{2} = f \frac{L}{d} \frac{\rho Q^2}{2 (\pi d^2)^2} \Rightarrow$$

$$f = \Delta p_f \frac{\pi^2 d^5}{8 L \rho Q^2} = \frac{0,74 \cdot 10^5 \pi^2 0,14^5}{8 \cdot 320 \cdot 10^3 \cdot 11^2}$$

$$f_a = 0,0314$$

$$Re = \frac{V d}{\nu} = \frac{Q \cdot d \cdot 4}{\pi d^2 \nu} = 7,5 \cdot 10^5$$

Moody-diagram, Fig 6.13, s. 318 \Rightarrow f är oberoende av Re .

b) $\therefore f_b = f_a$ enligt ovan

$$\Delta p_f = f_b \frac{L}{d} \frac{\rho V_b^2}{2} = 14,6 \text{ kPa}$$

Det räcker alltså inte att öka trycket p_1 till 170 kPa.



Givet: $U = 50 \text{ m/s}$

$$u(x_1, y_1) = u(x_2, y_2) = 42 \text{ m/s}$$

$$x_1 = 0,05 \text{ m} \quad x_2 = 2,5 \text{ m}$$

$$t = 20^\circ \text{C} \quad \nu = 15,2 \cdot 10^{-6} \text{ m}^2/\text{s}$$

$$p = 100 \text{ kPa} \quad \rho = 1,189 \text{ kg/m}^3$$

Sökt: y_1 och y_2

Lösning:

a) $x = x_1$

$$Re_{x_1} = \frac{U x_1}{\nu} = 1,64 \cdot 10^5 < Re_{x_{kr}} \Rightarrow \text{lam.}$$

$$\frac{u}{U} = \frac{42}{50} = 0,84 \quad \text{Tab. 7.1} \Rightarrow \eta = 2,96$$

$$y = \frac{\eta}{\sqrt{\frac{U}{\nu x}}} = 3,65 \cdot 10^{-4} \text{ m}$$

b) $x = x_2 \quad Re_{x_2} = 8,224 \cdot 10^6 > Re_{x_{kr}} = 5 \cdot 10^5$

\therefore turb gs. Antag omslag redan i framkanter

$$(7.43) \Rightarrow \tau_w = 0,135 \frac{\rho U^2}{\sqrt[3]{Re_x}} = 4,127 \text{ Pa}$$

$$u^* = \sqrt{\frac{\tau_w}{\rho}} = 1,863 \text{ m/s}$$

Antag log-lagen: $\frac{u}{u^*} = 2,44 \ln \frac{u^* y}{\nu} + 4,9$

$$\Rightarrow y = \frac{\nu}{u^*} e^{(\frac{u}{u^*} - 4,9)/2,44} = 0,0112 \text{ m}$$

Kontroll:

$$\frac{u^* y}{\nu} = 1382, \quad \text{log-lagen kan anses gälla}$$

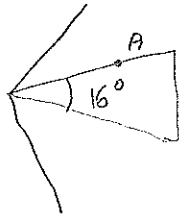
Svar a) $y = 0,37 \text{ mm}$ b) $y = 11,2 \text{ mm}$

P4 01+01-11

as $Ma = 3$

Luft $\Rightarrow k = 1,4$

\rightarrow
 $P = 70 \text{ kPa}$



För $Ma_1 = 3$; $\theta = 8^\circ$ ger ekv (9.86)

$$\tan \theta = \frac{2 \cot \beta (Ma_1^2 \sin^2 \beta - 1)}{Ma_1^2 (k + \cos 2\beta) + 2}$$

Iterering $\Rightarrow \beta = 25,61^\circ$

$$\frac{P_A}{P_1} = \frac{1}{k+1} [2k \cdot Ma_1^2 \sin^2 \beta - (k-1)] \quad (9.83a)$$

$$\Rightarrow \underline{P_A = 126 \text{ kPa}}$$

y: En normal stat förmas

$$\Rightarrow P_B = P_{02}$$

$$\text{Tabell B1} \Rightarrow P_{01} = P / 0,0272 \approx 2574 \text{ kPa}$$

$$\text{Tabell B2, } Ma = 3 \Rightarrow P_{02} / P_{01} = 0,3283$$

$$P_{02} = P_B = 0,3283 \cdot 2574 \text{ kPa} = \underline{845 \text{ kPa}}$$